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Advance Fluid

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①

Q No 1

Write down expression for velocity profile in laminar flow inside the pipe

As

$$h_f = \frac{f \cdot L}{2 \gamma}$$

from the viscosity  $\rightarrow \tau = \mu \frac{du}{dy}$

where  $u$  is velocity at distance "y" from boundary

Thus

$$y = r_0 - r$$

$$dy = \cancel{dr_0} - dr$$

$$dy = -dr$$

Thus

$$\tau = -\mu \frac{du}{dr}$$

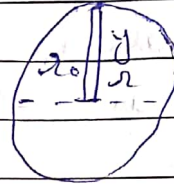
or

$$\int du = \int -\frac{h_f L \gamma}{2 \mu} \cdot r dr$$

$$u = -\frac{h_f L \gamma}{2 \mu} \cdot \frac{r^2}{2} + C$$

General Equation

Now applying boundary condition



$$U_{\max} = 0 + C$$

$$\therefore C = U_{\max}$$

Putting value in general Eq

$$\Rightarrow U = U_{\max} - \frac{h l \nu}{2 l l} \cdot \frac{r^2}{2}$$

$$U = U_{\max} - k r^2$$

$$k = \frac{h l \nu}{4 l l}$$

for  $r = r_0$ ,  $U = 0$

Thus

$$0 = U_{\max} - k r_0^2$$

$$U_{\max} = k r_0^2$$

Q.1 (2)

Define Critical Reynold Number

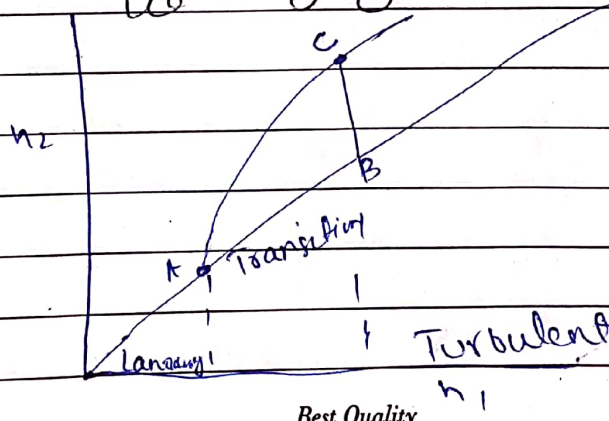
Critical Reynold Number:

If the head loss in given length of pipe is measured at different values of velocity it will be found that as long as velocity is low enough to secure laminar flow, the head loss due to friction will be directly proportional to

velocity but increase in velocity will change flow from laminar to turbulent causing change in head proportional to " $V^n$ "

where  $n$  varies from

1.75 to 2.0





The upper critical number corresponds to point B and depends on care taken to prevent initial disturbances.

It value is 4000 but it is impossible to achieve. The lower point A is more definite than higher one and it is known as true Reynolds number.

It value is 2000

$$R = \frac{D V \rho}{\mu}$$

(5)

M□□W□□□□□

H/W□-C/W□

Dated:...../...../20.....

Q No 2

GIVEN:

$$S = 0.7$$

$$V = 1.8 \times 10^{-5} \text{ m}^2/\text{s}$$

$$d = 15 \text{ mm} = 0.015 \text{ m}$$

$$Q = 0.5 \text{ l/s}$$

Required:

$$f = ? , T = ?$$

$$\text{velocity} = ?$$

0.0005

0.017

SOLUTION:

Check flow

$$R = \frac{DV}{\mu} \quad V = \frac{Q}{A} = \frac{0.001 \times 0.5}{\pi/4 (0.015)^2}$$

$$V = 0.029$$

$$R = \frac{0.015 \times 0.029}{1.8 \times 10^{-5}}$$

$$= 241 < 2000 \text{ laminar}$$

As

$$V_{av} = \frac{V_{cx}}{2}$$

$$V_{cx} = V_{av} \times 2$$

Best Quality

(6)

M T W T F S

H/W C/W

Dated: ...../...../20.....

$$V_{cr} = 0.029 \times 2$$

$$= 0.058$$

$$U = U_{max} - K \eta^2$$

$$\eta = 0.15$$

$$\text{When } \eta = \eta_0 = 0.075 \Rightarrow U = 0$$

Thus

$$U_{max} = K \eta_0^2$$

$$K = \frac{U_{max}}{\eta_0^2}$$

$$= \frac{0.058}{(0.075)^2} = \frac{0.058}{0.0056}$$

$$= 10.35$$

for Laminar  $f = \frac{64}{R}$

$$= \frac{64}{241}$$

$$= 0.265$$

(7)

MOTOWOTOFOS

H/W-C/W

Dated:...../...../20.....

$$J = \frac{f \cdot \rho \cdot V^2}{4 \cdot d}$$

$$= \frac{0.26 \times 0.7 \times 1000 \times (0.029)^2}{4 \cdot d}$$

$$= 0.065 \times 700 \times 0.00084$$

$$= 0.0388 \text{ N/m}^2$$

Velocity at 1mm from edges

$$U = U_{\max} - K r_0^2$$

$$= 0.058 - 10.35(0.01)^2$$

$$= 0.058 - 0.00135$$

$$= 0.056$$

At boundary or edges of Pipe

$$U_{\max} = 0 + C$$

$$\text{When } r = 0, U = U_{\max}$$

$$U_{\max} = 0.058$$

P-T-O



(8)

M T W T F S

H/W C/W

Dated: ...../...../20.....

Max Shear stress at wall of pipe

Maximum shear stress at wall of pipe is

$$\tau_0 = \frac{f}{8} \times P \times V^2$$

$$= \frac{0.26 \times 0.7 \times 1000 \times (0.029)^2}{8}$$

$$\tau_0 = 0.032 \times 700 \times 0.000841$$

$$= 0.018 \text{ N/m}^2$$