

Date:

□□-□□-□□

Name :- M. Mamoon

I.D :- 7690

Sec :- C

Semester :- 8<sup>th</sup> Summer

Dept :- BE (Civil)

Assignment :- Mid term

Submitted :- Sir. Abdul Waheed

Date :- 26.8.2020

Subject :- Adv. Fluid Mechanics

Date:

□□-□□-□□

Pg:- 1

Question :- 01 P(A)

Velocity Profile in laminar flow inside the pipe :-

→ For a circular Pipe :-

The laminar flow is defined to have the flow Reynolds number  $< 2000$

Reynolds Number :-

$$Re = \frac{\rho V D}{\mu} = \frac{V D}{\nu} < 2000$$

for laminar flow

→ Laminar Pipe flow :-

The shear stress laminar flow is linearly related the fluid viscosity.

$$\tau = \mu \frac{du}{dr}$$

Added by the above relation:

$$\mu \frac{du}{dr} = - \frac{r}{2} \frac{dp}{dx}$$

To Integrate the above yields.

$$\mu = \frac{1}{\mu} \frac{dp}{dx} \frac{r^2}{2} + C$$

The Integration constant  $C$  can be determined by  $\mu = 0$  at  $r = D/2$

(on solid boundary)

$$0 = \frac{1}{\mu} \frac{dp}{dx} \frac{r^2}{2} + C$$

Now for  $r = 0$ ,  $\mu = \mu_{max}$   
Putting values

$$\mu = \frac{-hLv}{2\mu L} \frac{r^2}{2} + C$$

$$\therefore \mu_{max} = 0 + C$$

$$C = \mu_{max}$$

Thus

$$\mu = \mu_{max} - \frac{hLv}{4\mu L} \cdot \frac{r^2}{2}$$

$\therefore$  velocity at any Point

$\Rightarrow$  Assume  $K = \frac{hLv}{4\mu L}$  ( $\mu = \mu_{max} - Kr^2$ )

As for  $r = r_0$ ,  $\mu = 0$

Date:

Pg: 3

$$0 = u_{max} - K \epsilon_0^2$$

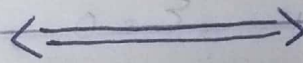
$$\text{or } u_{max} = K \epsilon_0^2 =$$

$$\frac{hLv}{4HL} = \epsilon^2$$

$g_0$  is also known critical velocity.

Now,

$$V_{av} = \frac{V_{eq} + 0}{2} = 0.5 V_{eq} \quad (\text{average velocity})$$



Question:- 01 P(B)

Critical Reynolds :-

Critical Reynolds number which decides whether flow is laminar or turbulent.

If head loss in given length of uniform pipe is measured at different values of velocity.

It will be found that as long as velocity is low enough to secure laminar flow, the head loss

due to friction will be directly proportional to velocity, but

increase in velocity, changes flow from laminar to turbulent

change in head loss. Thus if

values are plotted, lines ~~are~~

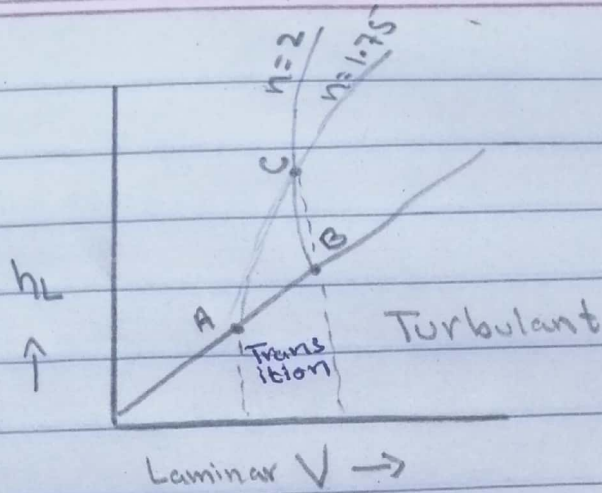
obtained with slope ranging

about 1.75 to 2.

Thus for laminar, drop of energy varies as  $v$  and for turbulent,

friction varies as  $v^n$  where  $n$

is 1.75 to 2.



The upper critical Reynolds number corresponding to point B is indeterminate and depends upon care taken to prevent initial disturbance. Its value is 4000. But normally, it's impossible for flow to be in straight line after  $R$  ~~flow~~ is at 2000. Thus lower value is much more definite than higher one and is dividing point. Thus lower value is true critical Reynolds number.

$$R = \frac{DVP}{\mu} = \frac{DV}{\nu}$$



(1)

Q2

Given Data:

Oil having  $S = 0.7$

Kinematic viscosity =  $1.8 \times 10^{-5} \text{ m}^2/\text{sec}$

Dia of Pipe =  $150 \text{ mm} = 0.15 \text{ m}$

Flow =  $0.5 \text{ L}/\text{sec} = 0.0005 \text{ m}^3/\text{sec}$ .

Required data:

Centerline velocity = ?

velocity at  $10 \text{ mm}$  from edge = ?

velocity at edge of pipe = ?

Max shear stress at wall = ?

Solution:

First we check the flow is  
Laminar or turbulent;

$$R = \frac{DV}{\nu} \rightarrow (1)$$

$$V = \frac{Q}{A} = \frac{Q}{\frac{\pi}{4} d^2} = \frac{0.0005}{\frac{\pi}{4} (0.15)^2}$$

(2)

$$V = 0.028 \text{ m/sec}$$

$$R = \frac{(0.15)(0.028)}{1.8 \times 10^{-5}}$$

$$R = 233.33 < 2000 \text{ (LAMINAR FLOW)}$$

$$V_{\text{av}} = 2V = 2 \times 0.028$$

$$V_{\text{av}} = 0.056 \text{ m/sec}$$

As:

$$u = U_{\text{max}} - ky^2$$

at

$$y = r_0 = 0.075 \text{ m}, \quad u = 0.$$

Thus

$$0 = U_{\text{max}} - ky^2$$

$$U_{\text{max}} = ky^2$$

$$k = \frac{U_{\text{max}}}{y^2} = \frac{0.056}{(0.075)^2}$$

$$k = 9.96$$



(3)

we get a equation;

$$u = 0.056 - 9.96 (r^2) \rightarrow *$$



→ velocity at 10 mm from edge

$$r = 0.065 \text{ m}$$

$$v = 0.056 - 9.96 (0.065)^2$$

$$\boxed{v = 0.014 \text{ m/sec}}$$

velocity at edge;

$$r = 0.075 \text{ m}$$

$$v = 0.056 - 9.96 (0.075)^2$$

$$v = -0.00002 \text{ m/sec} \quad \text{Say } v = 0$$

Similarly:

$$f = \frac{64}{R} = \frac{64}{233.33}$$

$$\boxed{f = 0.27}$$

(4)

Shear stress at wall ;

$$\tau = \frac{f}{4} \rho \frac{v^2}{2}$$

$$= \frac{0.27}{4} \times (0.7 \times 1000) \times \frac{(0.056)^2}{2}$$

$$\tau = 0.074 \text{ N/m}^2$$

Ans