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Question no:01

A prototype gate valve which will control the flow in a pipe system conveying Paraffin is to be studied in model. List the significant variables on which the pressure drop across valve would depend.

Perform dimensional analysis to obtain the relevant non-dimensional groups.

A  $1/5$  Scale model is built to determine the pressure drop across the valve with water as the working fluid.

Part (a): - - - - -

Part (b): - - - - -

Part (c): - - - - -

(The density and viscosity of paraffin are  $800 \text{ kg} \cdot \text{m}^{-3}$  and  $0.002 \text{ kg} \cdot \text{m}^{-1} \cdot \text{s}^{-1}$  respectively. Take the kinematic viscosity of water as  $1.0 \times 10^{-6} \text{ m}^2 \cdot \text{s}^{-1}$ ).

Solution: The pressure drop  $\Delta P$  is expected to depend upon the gate opening  $h$ , the overall depth  $d$ , the velocity  $v$ , density  $\rho$  and viscosity  $\mu$ .



⇒ list the relevant variables:

$$\Delta p, h, d, V, \rho, \mu$$

⇒ writing down dimensions:

$$\Delta p \rightarrow ML^{-1}T^{-2}$$

$$h \rightarrow L$$

$$d \rightarrow L$$

$$V \rightarrow LT^{-1}$$

$$\rho \rightarrow ML^{-3}$$

$$\mu \rightarrow ML^{-1}T^{-1}$$

Number of variables:  $n=6$

Number of independent dimensions:  $m=3$  (M, L and T)

Number of non-dimensional groups:  $n-m=3$

Choose  $m(=3)$  Scaling variables:

geometric ( $d$ ); kinematic (time-dependant ( $V$ )); dynamic mass dependent ( $\rho$ ).

Form dimensionless groups by non-dimensionalising the remaining variables:  $\Delta p, h$  and  $\mu$ .

$$\pi_1 = \Delta p d^a V^b \rho^c$$

$$\begin{aligned} M^0 L^0 T^0 &= (ML^{-1}T^{-2})(L)^a (LT^{-1})^b (ML^{-3})^c \\ &= M^{1+c} L^{-1+a+b-3c} T^{-2-b} \end{aligned}$$

$$M = 0 = 1+c \quad \Rightarrow c = -1$$

$$T = 0 = -2-b \quad \Rightarrow b = -2$$

$$L = 0 = -1+a+b-3c \quad \Rightarrow a = 1+3c-b=0$$

$$\Rightarrow \pi_1 = \Delta P V^{-2} \rho^{-1} = \frac{\Delta P}{\rho V^2}$$

$$\pi_2 = \frac{h}{d} \quad (\text{by inspection, since } h \text{ is a length})$$

$$\pi_3 = \mu d^a V^b \rho^c \quad (\text{probably obvious by now, but here goes anyway})$$

$$\begin{aligned} M^0 L^0 T^0 &= (M L^{-1} T^{-1}) (L)^a (L T^{-1})^b (M L^{-3})^c \\ &= M^{1+c} L^{-1+a+b-3c} T^{-1-b} \end{aligned}$$

$$M \Rightarrow 0 = 1+c \quad \Rightarrow \boxed{c = -1}$$

$$T \Rightarrow 0 = -1-b+0 \quad \Rightarrow \boxed{b = -1}$$

$$L \Rightarrow 0 = -1+a+b-3c \quad \Rightarrow a = 1+3c-b \quad \boxed{-1}$$

$$\Rightarrow \pi_3 = \mu d^{-1} V^{-1} \rho^{-1} = \frac{\mu}{\rho V d}$$

Recognition of Reynolds number suggests that we replace  $\pi_3$  by

$$\pi'_3 = (\pi_3)^{-1} = \frac{\rho V d}{\mu}$$

$\Rightarrow$  Hence dimensional analysis yields:

$$\pi_1 = f(\pi_2, \pi'_3)$$

$$\text{i.e. } \frac{\Delta P}{\rho V^2} = f\left(\frac{h}{d}, \frac{\rho V d}{\mu}\right)$$

(a) Dynamic similarity requires that all non-dimensional group be the same in model and prototype; i.e.

$$\pi_1 = \left(\frac{\Delta P}{\rho V^2}\right)_p = \left(\frac{\Delta P}{\rho V^2}\right)_m$$

$$\pi_2 = \left(\frac{h}{d}\right)_p = \left(\frac{h}{d}\right)_m \Rightarrow (\text{automatic of similar shape})$$



$$\pi'_3 = \left( \frac{\rho u d}{\mu} \right)_p = \left( \frac{\rho u d}{\mu} \right)_m$$

⇒ From the last, we have a velocity ratio

$$\frac{U_p}{U_m} = \frac{(\mu/\rho)_p}{(\mu/\rho)_m} \frac{d_m}{d_p} = \frac{0.002/800}{1.0 \times 10^{-6}} \times \frac{1}{5} = 0.5$$

Hence 
$$U_m = \frac{U_p}{0.5} = \frac{3.0}{0.5} = 6.0 \text{ ms}^{-1}$$

(b) The ratio of quantities of flow is

$$\frac{Q_p}{Q_m} = \frac{(\text{velocity} \times \text{area})_p}{(\text{velocity} \times \text{area})_m} = \frac{U_p}{U_m} \left( \frac{d_p}{d_m} \right)^2 = 0.5 \times 5^2 = 12.5$$

(c) Finally for the pressure drop,

$$\pi_1 = \left( \frac{\Delta P}{\rho U^2} \right)_p = \left( \frac{\Delta P}{\rho U^2} \right)_m \Rightarrow \frac{(\Delta P)_p}{(\Delta P)_m} = \frac{\rho_p}{\rho_m} \left( \frac{U_p}{U_m} \right)^2 = \frac{800}{1000} \times 0.5^2$$

Hence 
$$\Delta P_p = 0.2 \times \Delta P_m = 0.2 \times 60 = 12.0 \text{ kPa}$$

Question no: 02

Design a practice profile of gravity dam with the following data:

- ① Max. depth of water in reservoir is ( $78\text{m} = H$ )
- ② Specific gravity of dam material is ( $G = 2.5$ )
- ③ Allowable compressive strength for the dam masonry is ( $786 \text{ T/m}^2$ )
- ④ Height of wave is  $H_w = 1.5\text{m} =$
- ⑤  $G$  and  $H_w$  is your own choice but differ from others.

Given Data:

~~XXXX~~ \*  $H = 78\text{m}$

\*  $G = 2.5$

\*  $\sigma_{all} = 786 \text{ T/m}^2$

\* Height of wave =  $H_w = 1.5\text{m}$

\*  $u =$

\* No uplift Pressure =  $C_u = 0$

Given Requirement: Design of practice profile of gravity dam.

Solution:

$$H_{\text{limiting}} = \frac{\sigma_{all}}{\gamma_w(G - C_u + 1)} = \frac{786 \times 1000}{(1000)(2.5 - 0 + 1)}$$

$$H_{\text{limiting}} = 224.57\text{m} > H_{\text{dam}} = 78\text{m}$$



⇒ Hence the dam is low gravity dam.

② Top width (a):

$$\text{Free board} = 1.5 * H_w$$

$$\text{Free board} = 1.5 * 1.5$$

$$\boxed{\text{Free board} = 2.25\text{m}}$$

$$\text{Height of Dam} = HD = H_w + \text{F.B}$$

$$HD = 78 + 2.25$$

$$\boxed{HD = 80.25\text{m}}$$

$$a = 14\% \text{ of } HD$$

$$a = \frac{14}{100} * 80.25$$

$$\boxed{a = 11.235\text{m}}$$

③ Base width "b" (without offset)

① For no sliding criteria:

$$b' = \frac{H_w}{\mu \cdot G} = \frac{78}{0.7 * 2.5}$$

$$\boxed{b' = 44.571 \approx 45\text{m}}$$

② For no tension Criteria:

$$b' = \frac{H}{\sqrt{G}} = \frac{78}{\sqrt{2.5}}$$

$$\boxed{b' = 49.33\text{m}}$$

$$\text{Using } \boxed{b' = 49.33\text{m}}$$

④ Depth of vertical portion on U/s side:

$$h' = 2a \sqrt{G - C_u}$$

$$h' = 2 \times (11.235) \sqrt{2.5 - 0}$$

$$h' = 35.53 \approx 36 \text{ m}$$

⑤ Upstream offset =  $\frac{a}{16}$

$$= \frac{11.235}{16}$$

$$= 0.70 \text{ m}$$

⑥ Depth below the water level to the end of inclined portion in U/s =  $3.14 \times a \sqrt{G}$

$$= 3.14 \times 11.235 \sqrt{2.5}$$

$$= 55.78 \text{ m}$$

⑦ Total width of the base of dam

$$b = b' + \frac{a}{16}$$

$$b = (49.33) + (0.70)$$

$$b = 50.03 \text{ m}$$

⑧  $\tan \theta = \frac{b'}{H} = \frac{49.33}{78}$

$$\theta = \tan^{-1} \left( \frac{49.33}{78} \right)$$

$$\theta = 32.31^\circ$$



(a) Depth of verticle portion on D/s (from WL on U/s side)

$$\tan \theta = \frac{a}{d'} = \frac{11.235}{d'}$$

$$\frac{49.33}{78} = \frac{11.235}{d'} \Rightarrow (d')(0.6324) = 11.235$$

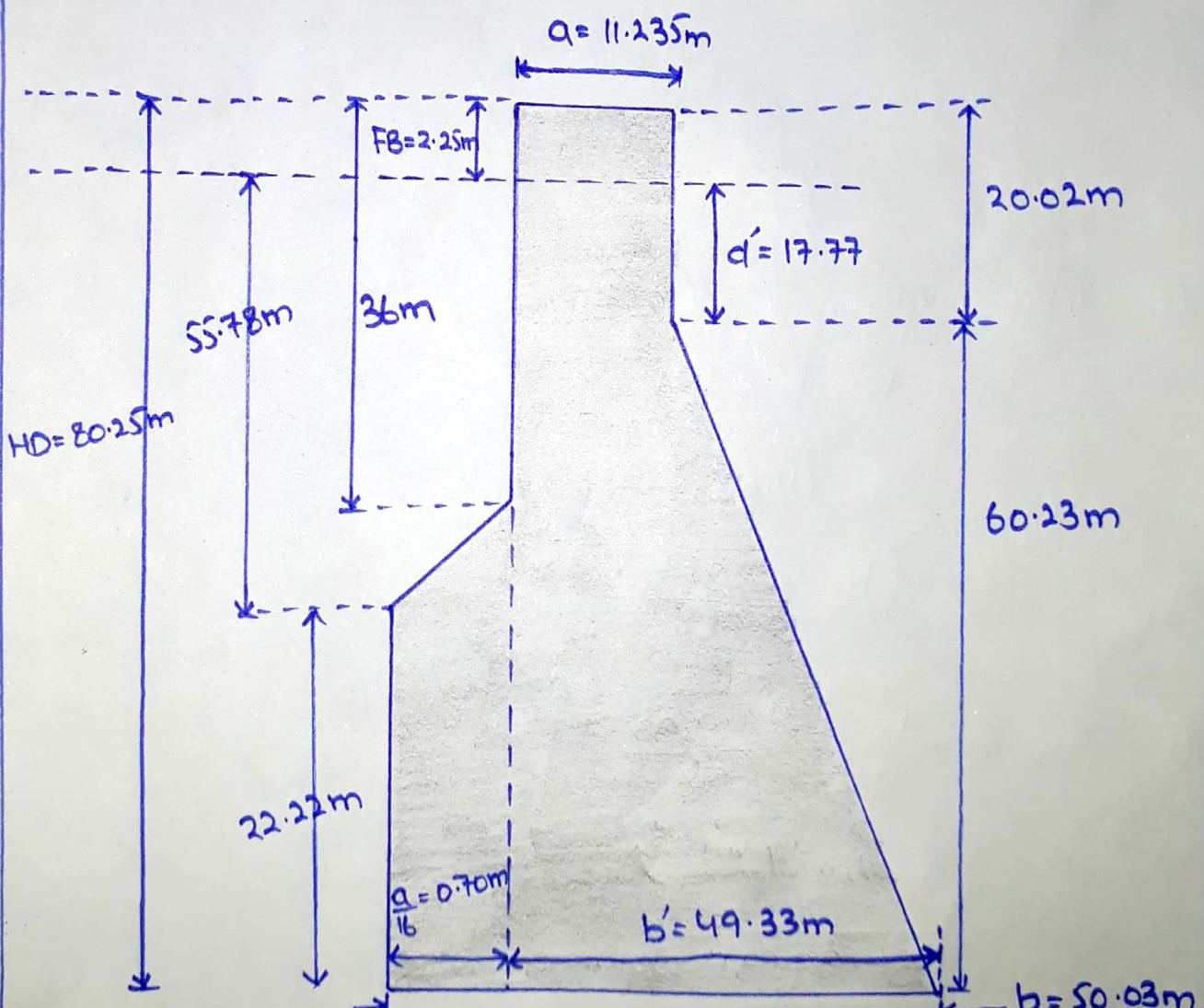
$$d' = \frac{11.235}{0.6324}$$

$$d' = 17.77 \text{ m}$$

Depth of verticle portion:

$$d = d' + F.B = 17.77 + 2.25$$

$$d = 20.02 \text{ m}$$



Question no: 03



Using any hydraulic model and explain the concept of Dimensional analysis and Similitude. Each student should have separate model analysis.

Ans: Dimensional Analysis: It is a mathematical technique making use of study of dimensions. It deals with the dimensions of physical quantities involved in the phenomenon.

⇒ In dimensional analysis, one first predicts the physical parameter that will influence the flow and then by grouping these parameters in dimensionless combinations a better understanding of flow is made possible.

Similitude: It is similarity between model and prototype in every respect which mean model and prototype have similar properties or model and prototype are completely similar.



Model: Spillways

⇒ The discharge per unit crest length of rectangular

weir could be expressed as:

$$Q = g^{1/2} H^{3/2} \phi \left[ \frac{\rho g^{1/2} H^{3/2}}{\mu}, \frac{\rho g H^2}{\sigma}, \frac{P}{H} \right]$$

⇒ The governing equation for spillways and weirs is identical. Flood discharges over spillways will result in very high Reynolds numbers, and since surface tension effects are also negligible the only factor effecting the discharge coefficient is  $P/H$ . In modeling dam spillways, therefore if the ratio of  $P/H$  in the model and prototype are identical and the crest geometry is correctly scaled.

$$\frac{Q}{g^{1/2} H^{3/2}} = \text{Constant}$$

Therefore, spillways model are operated according to the Froude law and are made sufficiently large that viscous and surface tension effects are negligible.

$$\left( \frac{V}{\sqrt{gt}} \right)_m = \left( \frac{V}{\sqrt{gt}} \right)_p$$

$$Q = V \ell^2$$

$$\Rightarrow \left( \frac{Q}{\ell^{5/2}} \right)_m = \left( \frac{Q}{\ell^{5/2}} \right)_p$$

where

$$Q_m = 1000 \left( \frac{1}{25} \right)^{5/2} = 0.32 \text{ m}^3/\text{s}$$

From Equation (ii)

$$V_p = V_m \sqrt{\frac{l_p}{l_m}} = V_m \sqrt{25}$$

$$\Rightarrow V_p = 1.5 * 5 = \boxed{7.5 \text{ m/s}}$$



Question no: 04

what will be the effect of Sediment Particle diameter, Particle density, Particle concentration, Particle Shape, viscosity of water, turbulence of water flowing in reservoir on Fall velocity? Explain in detail.

Ans: The following will be the effect of Sediment on the Fall velocity:

(i) Particle Diameter: The particle diameter or size of particle have a significant effect on the Fall velocity.

⇒ The larger particles will settle more quickly as compared to the particles having small size. It is

according to the principles of Stokes law.

⇒ Hence Particle Fall or Settling is directly proportional to Fall velocity.

(ii) Particle Density: Those particles which have high density

will settle down more faster than those particles of low density, with same sizes, will settle slower.

⇒ when pulp density is below 2% solids, free settling behavior occurs and settling is much faster than when

pulp density is high (Hindered settling). These terms also

apply the Centrifugal classification in hydrocyclones and Centrifuges.

(iii) Particle Shape: Particle Shape has a major effect on settling - a sphere settles much faster than a cube of the same relative size and S.G. Some particles are shaped like flakes - these settle much slower than a particle of same relative size and Specific Gravity (S.G.).

\* The greater the settling of a particle, the greater will be the fall velocity.

(iv) Viscosity of water: The water having high viscosity will offer more resistance to the particles to settle down and hence there will be less particles settled in more viscous water and hence the fall velocity will be low due to high viscosity of water.

(v) Particle Concentration: when a suspended concentration of sediment increases, the settling velocity of each particle decreases due to the modification of the flow induced by previous particles.

⇒ Hence Particle Concentration have direct relation with fall velocity.



(vi) Turbulance of water: At high turbulence intensity the relative settling velocities increases with the increasing relative turbulence intensity regardless of the Stoke number. At the ~~large~~ intermediate turbulence intensity, it seems that the settling bifurcate.

The particles at the large Stokes number tend to be slowed, whereas the settling velocity of particles is increased at a small Stokes number.