

M T W T F S

H/W C/W

Dated:/...../20.....

Name: M Kamran

IDNO : 7888

Semester : 6th

Question: 1

Define Drag with its components
write down the equation
for friction drag coefficient
both in laminar & turbulent
boundary layers.

Ans:

Force on Immense Body:

A body in
whole immense in a
homogeneous fluid may
be subject to two
kind of forces arising
from relative motions
b/w body and fluid.
These forces are
termed as drag
force depending whether
at right angle or
motion.

Drag forces as submerged
body can have
two components.

Pressure Drag Force:

It is equal
to the integration of
component in the direction

of motion of all pressure
 forces the surface of body on

$$F_p = C_p \frac{\rho v^2}{2} A$$

C_p depend on shape

Friction Drag:

It is equal to integration of shear stress along the surface of the body in direction of motion.

$$F_f = C_f \frac{\rho v^2}{2} BL$$

C_f : depend on viscosity

Friction Drag of Boundary layer:

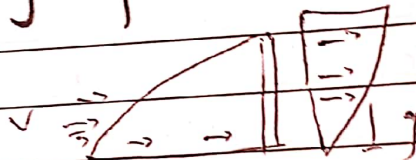
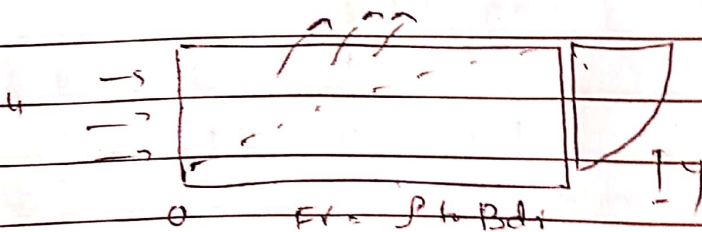


Figure show growth of the boundary layer along one side of smooth plate is steady from incompressible fluid consider in central volume.



(3)

MOTOWTOS

H/W-C/W

Dated:...../...../20.....

where p is distance from boundary layer to plate.

Now $F_x = \text{drag} = \text{rate of momentum in } x \text{ direction leaving through BC}$

\Rightarrow rate of momentum in x direction leaving through AB. momentum in x direction leaving along OA

Impulse Moment Principle.

$$\sum F = \frac{d(mu)}{dt} = \rho \times v \times v = \int \rho v$$

$$\sum F_x = \int \rho v_2 v_2 - \rho v_1 v_1$$

$$DA \rightarrow \rho v (v \times B \times p)$$

$$CB \rightarrow \rho B \int_0^B u^2 dy$$

$$AB \rightarrow \rho (v \times B \times (-B \int_0^B u dy)) v$$

Putting value

$$F_x = \rho B \int_0^B u (u - v) dy$$

Solving this equation

$$F_x = \rho B v^2 \delta^* \quad \text{where } \delta^*$$

the function of boundary layer velocity condition

(4)

MOTOWOTOFOS

H/W C/W

Date: / / 20

distribution

Now to find local
wall shear stress

$$\tau = \frac{F_x}{\text{Area}} = \tau_0 = \frac{dF_x}{B dx}$$

$$F_x = \rho B V^2 \delta x$$

$$F_x = \rho V^2 \times \frac{d\delta}{dx}$$

$$\tau_0 = \rho V^2 \times \frac{d\delta}{dx}$$

Laminar Boundary Layer

In case of laminar

$$\tau_0 = \mu \left(\frac{du}{dy} \right)_{y=0} = \frac{\mu}{\rho} \left(\frac{du}{dx} \right) = \frac{\mu V}{\rho} \left(\frac{dF(x)}{dx} \right)$$

By solving

$$\tau_0 = \frac{\mu V}{\rho} \quad \text{--- (1)}$$

Equating

$$\tau_0 = \rho V^2 \times \frac{d\delta}{dx}$$

$$\rho V^2 \times \frac{d\delta}{dx} = \frac{\mu V}{\rho} \quad \frac{d\delta}{dx} = \frac{\mu}{\rho V}$$

Solving it

$$\frac{\delta^2}{2} = \frac{\mu V x}{\rho V^2} + C$$

(5)

Date:/...../20.....

MOTOWOTIFOS

H/W-C/W

At $x=0$, $P=0$, $c=0$

$$\delta = \sqrt{\frac{2\mu B}{\rho u}} = \sqrt{\frac{2\beta \cdot x}{R_x}} \quad R_x = \frac{\rho u x P}{\mu}$$

Experimentally

$$\delta B = 1.63, \quad x = 0.135$$

$$\frac{\delta}{x} = \sqrt{\frac{2 \times 1.63}{0.135}} \times \frac{1}{\sqrt{R_x}} = \frac{4.91}{\sqrt{R_x}}$$

where R_x may be called
 the local Reynolds number
 It should be noted
 that R_x increase linearly
 in down stream direction

Now

$$F_p = B \int_0^x \delta^2 Z_0 dx$$

$$Z_0 = 0.332 \frac{\mu v}{x} \sqrt{R_x}$$

$$R_x = \frac{\rho u x P}{\mu}$$

Thus

$$F_p = 0.6648 \sqrt{\rho \mu L U^3}$$

$$F_p = C_F \frac{\rho v^2 B L}{B}$$

$$C_F = 1.328 \sqrt{\frac{\mu}{\rho L V}} = \frac{1.328}{\sqrt{R}} \quad \text{---}$$

where R is based on characteristics length of whole plate. The laminar boundary layer will remain laminar if R_x is about 500,000

Part B.

Derive equation for critical depth, critical velocity of a rectangular section of a channel.

Ans

Specific Energy:

defined as the energy head referred to channel bed to datum.

$$E = y + \frac{v^2}{2g}$$

channel is uniform depth and relatively wide, flow near center of

(7)

M T W T F S

H/W C/W

Dated:/...../20.....

Channel will be unaffected
by side boundaries

Flow q per unit width

$$q = \frac{\phi}{y}$$

Now average velocity

$$V = \frac{\phi}{A} = \frac{qy}{by} = \frac{q}{y}$$

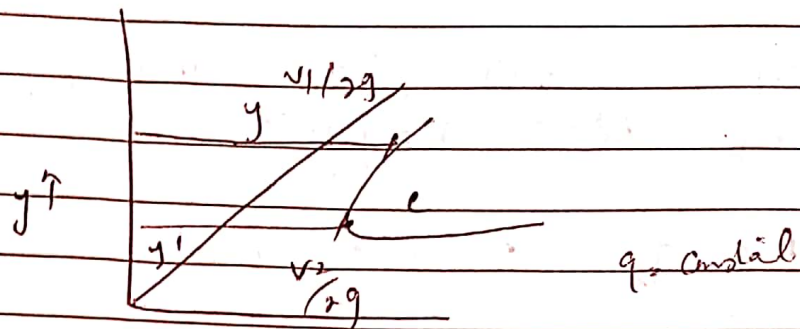
Thus $E = y + \frac{1}{g} \left(\frac{q^2}{y^2} \right)$

Consider how E will vary
with y if q remains
constant

$$(E - y) = \frac{q^2}{2g(y^2)}$$

$$(E - y)y^2 = \frac{q^2}{2g} = \text{constant}$$

Plot of E vs y is
parabola



This specific energy diagram

From particular q , there will be two kind of possible values of y for given E . The equation is cubic with three roots with third root being negative giving no value.

This two alternate depth represent two totally different flow regimes: slow and deep portion and fast & shallow on lower portion. This divide b/w two regimes of flow.

The relation of critical depth can be found as

(9)

M T W T F S

H/W C/W

Dated:/...../20.....

$$E = y + \frac{1}{2g} \left(\frac{q^2}{y^2} \right)$$

minimum spec energy $\frac{dE}{dy} = 0$

$$\frac{dE}{dy} = 1 + \frac{2}{2g} \left(\frac{q^2}{y^2} \right)$$

$$\frac{dE}{dy} = 1 - \frac{q^2}{gy^3} = 0$$

$$1 = \frac{q^2}{gy^3} \Rightarrow q^2 = gy^3 \text{ or } \frac{q^2}{g} = y^3$$

$$q^2 = gy^3 \Rightarrow y_c = \left(\frac{q^2}{g} \right)^{1/3}$$

$$q_c \text{ Vay :- } V_c^2 = gy_c$$

$$y_c = \frac{V_c^2}{g}$$

$$E_{\min} = y_c + \frac{V_c^2}{2g} = y_c + \frac{y_c}{2}$$

$$= \frac{3}{2} y_c$$

Question: 2

Find the depth of rectangular
 depth of water flows
 at the rate of
 $3.5 \text{ m}^3/\text{s}$ with bed slope
 of 0.0008 and $n = 0.0219$
 width of bed in your
 student ID number.

Also find critical depth,
 critical velocity -

Is flow sub critical - super
 critical?

Given data

$$Q = 3.5 \text{ m}^3/\text{s}$$

$$S_0 = 0.0008$$

$$n = 0.0219$$

$$b = 7888 \text{ mm}$$

Required.

$$y = ?$$

$$y_{cr} = ?$$

$$V_{cr} = ?$$

$$Q = \frac{1}{n} \cdot A \cdot R_m^{2/3} \cdot S^{1/2}$$

$$A = y \cdot b$$

$$= y \times 7.888$$

$$R_m = \frac{A}{P}$$

$$= \frac{7888}{2415.694}$$

Putting values

$$3.5 - 1 \times 7888 \times \left(\frac{7888}{2415.694} \right)^{2/3} (0.0008)^{1/2} = 0.0219$$

$$y = 0.7222 \text{ m}$$

$$y = 722.8 \text{ mm}$$

Now

$$y_{cr} = \left(\frac{q^2}{g} \right)^{1/3}$$

$$q = \frac{Q}{b} = \frac{3.5}{7888} = 0.446 \text{ m}^2/\text{s}$$

$$y_{cr} = 0.2720 \text{ m}$$

$$y_{cr} = 272.6 \text{ mm}$$

(12)

M T W T F S

H/W C/W

Dated:/...../20.....

$$V_{cr} = 2$$

$$V_{cr} = \sqrt{g y_{cr}}$$

$$V_{cr} = \sqrt{9.81 \times 0.272}$$

$$V_{cr} = 1.63 \text{ m/s}$$

Since

$$V > V_{cr}$$

Flow is subcritical

No 3:

Find friction drag on one side of a smooth plate with 200mm wide and 800mm length placed specific gravity of 0.89. The undisturbed velocity is 5m/s and kinematic viscosity is $0.93 \times 10^{-4} \text{ m}^2/\text{s}$.

Given Data:

$$\text{width} = 200 \text{ mm}$$

$$L = 800 \text{ mm}$$

$$\text{Specific gravity} = 0.89$$

$$U = 5$$

$$V = 0.93 \times 10^{-4} \text{ m}^2/\text{s}$$

Solution

$$R = \frac{LU}{V}$$

$$V = 0.93 \times 10^{-4} \text{ m}^2/\text{s}$$

$$L = 0.80$$

$$U = 5$$

Put values

$$\frac{0.80 \times 5}{0.93 \times 10^{-4}}$$

$$= 43010 < 500,000$$

Thus

$$C_f = \frac{1.328}{\sqrt{R}}$$

$$\Rightarrow \frac{1.328}{\sqrt{43010}} = 0.0064$$

$$F_f = C_f \rho \frac{V^2}{2} \times BL$$

$$F_f = 0.006 \times 0.89 \times 1000 \times \frac{(5)^2}{2} \times 0.20 \times 0.80$$

$$\Rightarrow 53.4$$

To find thickness of
Boundary Layer.

$$\frac{\delta}{x} = \frac{4.91}{\sqrt{Re}} \quad \text{at } x=L$$

$$\delta = \frac{4.91}{\sqrt{43010}} \times 80 \text{ cm}$$

$$\delta = 1.89 \text{ cm}$$

$$F_f = 0.664 \times 8 \sqrt{\rho \cdot V \cdot L \cdot \mu}$$

$$0.664 \times 0.20 \sqrt{0.89 \times 1000 \times (1000 \times 0.39 \times 0.934 \times 10^{-3})^2 \times 0.8 \times (5)^3}$$

$$F_f = 11.39 \text{ N} \quad \text{Answer}$$